



Software for the simulation, troubleshooting and operations of gas or oil fired process heaters.

Overview

FIHR™ is a simulation program for fireboxes and convection sections of fired process heaters. In simulation mode, it can be used for troubleshooting, such as identification of tube burnout, and operation, to identify the best operating conditions given changes in feedstock or product specifications.

Key performance variables, such as product and metal temperatures are presented graphically, to enable rapid evaluation of operational changes, including the effect of flame shape and heat release.

Features

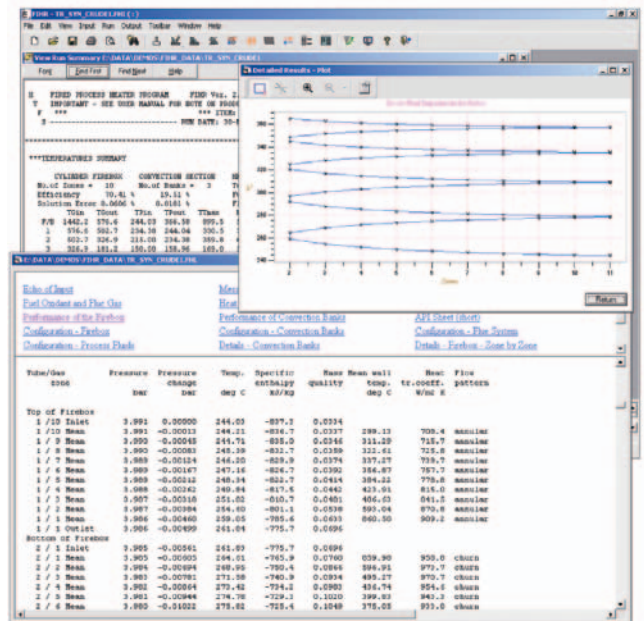
Operating Modes

The following operating modes are available, providing specific capabilities based on the task being performed:

- Simulation
- Burner rating

Technical Summary

- Process Applications
 - Single-phase liquids or gases or boiling liquids for all or part of their duty
 - Both pure component (isothermal) liquids and mixtures
 - Up to 10 streams may pass through several different parts of the heater and the firebox stream may be pre-heated in the convection section tube banks
 - User can specify process- and gas-side fouling, in any section
- Calculations Methods
 - Calculates the process outlet conditions for all process streams in the heater, in addition calculating the flue gas draft
 - A 'burner rating' mode calculates the required fuel flowrate for a defined outlet condition of the main firebox process
 - Firebox radiation modeled by 'well stirred' (single zone) or 'long furnace' (up to 20 longitudinal zones) methods. HTFS® models for typical industrial burner heat release
 - Considers radiation heat transfer in the tube banks
 - Circumferential heat flux and peak tube wall temperature based on API 530
- Geometry
 - Cylindrical fireboxes containing vertical hairpin tubes or a refractory backed helical coil
 - Cabin fireboxes (single or twin), with vertical or horizontal tubes, which may be wall-mounted or centrally located, (in single or double rows) with firing on both sides
 - Open or ducted flue gas systems with an air pre-heater with ID and FD fans if required
 - May also be used for a standalone convection section or heat recovery train
 - Up to 9 convection section tube banks with plain or extended (fins or studs) surfaces
 - Tubes of different diameter and separation; tubes with U-bends inside or outside the firebox
 - Extensive help, including firebox and tube bank diagrams to aid input



- Output
 - Summary of heater performance
 - API fired heater datasheet
 - Detailed thermal analysis of each part of the heater including, estimate of maximum metal temperatures, process-side film and tube wall temperatures
 - Graphical output of process and flue gas temperature, heat transfer rate, process temperature, tube metal temperature profiles, heat transfer coefficient variation and draft
- Program integration – link to HYSYS® and Aspen Plus™

Benefits

- **Improved design** – FIHR is a comprehensive, easy-to-use tool for the design of fired process heaters. Its use enables the more efficient design of new heaters and cost-effective revamp studies. It can also augment or replace in-house tools that are difficult to use and expensive to maintain and update.
- **Improved process operations** – Links to process simulators allow the effect of phenomena such as pre-heat exchanger fouling, to be properly evaluated. Major operational savings can be made with the use of a comprehensive heater model based on sound firebox radiation modeling providing a rational basis for day-to-day optimization of plant performance with changing product specifications, feedstock changes. The rigorous modeling of FIHR is vital for proper investment appraisal where retrofit process modifications are proposed to optimize product yields.
- **Increased engineering efficiency** – In many processes, operation of fired heaters can be a limiting step, as these are often run at the practical limit of firebox tube temperature. In a reactor charge heater, one customer was able to use FIHR to explore a range of fouling assumptions. He developed a relationship between stack temperature and a safe working limit for the tubes and was able to predict the throughput reduction with time. This enabled the cleaning cycle to be optimized for throughput versus downtime and decoke costs, resulting in savings of several hundred thousand dollars.

Mass or Molar Compositions	Fuel 1 default (mass)	Fuel 2 Molar flows/l	Fuel 3 Molar flows/l	Fuel 4 default (mass)
Methane		0.7	0.05	
Ethane		0.15		
Propane		0.105		
Butanes		0.035		
Perlanes				
Hexanes				
Cyclohexane				
Benzene				
Ethene				
Propene				
Butenes				
Perkenes				
Butadienes				
Acetylene				
Hydrogen			0.25	
Hydrogen sulphide				
Ammonia				
Oxygen				
Nitrogen		0.009	0.4	
Argon				
Water vapour				

HTFS Data Browser - Firebox Tube Layout

Tube Orientation in: Vertical tubes | No. of Paths through Firebox Tubes: 5

Min. of Tubes in a Path: 1 | Tube Path Layout #: FIHR default

Tube straight line length: 13.5 m | Tube to wall clearance: 100 mm

Height from floor to first tube: 0.2 m | Number of bends in Heat Transfer Area: Yes

Cool Diameter: m

HTFS Data Browser - Fuels

Fuel Type Identifiers	Units	Fuel 1 NonStoichCo	Fuel 2 Stoich	Fuel 3 Stoich	Fuel 4 Not set
Fuel Flowrate	kg/h	100	200	50	
Fuel Temperature	°C	20	20	20	

HTFS Data Browser - Results

Final calculations started: FIHR SIM on 30-MAY-2003 09:37

Output of results began: BEGINNING OF SIM 1

FIHR successfully completed

For help, press F1 | C:\nc\Firebox\links | 1022



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